



UNIVERSITY OF NAPLES FEDERICO II 1224 A.D.

Propulsione Aereospaziale

T. Astarita astarita@unina.it www.docenti.unina.it

Versione del 31.5.2019

Cenni sul sistema tecnico Americano





Cenni sul sistema tecnico Americano





Lunghezze

| Unità | Divisioni | Equivalente SI |
|------------------------------------|----------------------------------|----------------------------------|
| Relazior | ni esatte in grassetto | |
| Iı | nternazionale | |
| 1 <i>punto</i> (point, p) | | 352,777 778 µm |
| 1 <i>pica</i> (pc ^[9]) | 12 p | 4,233 333 mm |
| 1 <i>pollice</i> (inch, in) | 6 рс | 25,4 mm |
| 1 <i>piede</i> (foot, ft) | 12 in | 0,304 8 m ^[10] |
| 1 <i>iarda</i> (yard, yd) | 3 ft | 0,914 4 m ^[10] |
| 1 <i>miglio</i> (mile, mi) | 5 280 ft o 1 760 yd | 1,609 344 km |
| Nautic | a internazionale ^[10] | |
| 1 braccio(fathom, ftm) | 2 yd | 1,828 8 m |
| 1 cable (cb) | 120 ftm o 1.091 fur | 219,456 m |
| 1 miglio nautico (NM o nmi) | 8.439 cb o 1.151 mi | 1,852 km |



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| Volume liquido | | | | | | | | | | |
|----------------------------|------------------------------|------------------------|--|--|--|--|--|--|--|--|
| Unità di r | nisura molto comun | i in <i>corsiv</i> o | | | | | | | | |
| Conve | ersione esatta in gra | assetto | | | | | | | | |
| Unità | Divisioni | Equivalente SI | | | | | | | | |
| 1 minim (min) | | 61,611 519 921 875 μL | | | | | | | | |
| 1 dramma liquida | | | | | | | | | | |
| (US fluid dram, fl dr) | 60 min | 3,696 691 195 312 5 mL | | | | | | | | |
| 1 cucchiaio da tè | | | | | | | | | | |
| (<i>teaspoon</i> , tsp) | 80 min | 4,928 921 593 75 mL | | | | | | | | |
| 1 cucchiaio da tavola | | | | | | | | | | |
| (<i>tablespoon,</i> Tbsp) | 3 tsp | 14,786 764 781 25 mL | | | | | | | | |
| 1 oncia liquida | | | | | | | | | | |
| (US fluid ounce, fl oz) | 2 Tbsp | 29,573 529 562 5 mL | | | | | | | | |
| 1 cicchetto(US shot, jig) | 3 Tbsp | 44,360 294 343 75 mL | | | | | | | | |
| 1 US gill (gi) | 4 fl oz | 118,294 118 25 mL | | | | | | | | |



| | Volume liquido | | | | | | | | | | | | |
|---|--|----------------------|--|--|--|--|--|--|--|--|--|--|--|
| Unità di I | misura molto comuni | i in <i>corsiv</i> o | | | | | | | | | | | |
| Conve | ersione esatta in gra | assetto | | | | | | | | | | | |
| Unità | Divisioni | Equivalente SI | | | | | | | | | | | |
| 1 <i>tazza (US cup</i> , cp) | 2 gi o 8 fl oz | 236,588 236 5 mL | | | | | | | | | | | |
| 1 <i>pinta</i> (<i>US liquid pint</i> , pt) | 2 ср | 473,176 473 mL | | | | | | | | | | | |
| 1 <i>quarto</i> (<i>US liquid quart</i> , qt) | 2 pt | 0,946 352 946 L | | | | | | | | | | | |
| 1 <i>gallone</i> (<i>US liquidgallon</i> , gal) | 4 qt o 231 in ³ | 3,785 411 784 L | | | | | | | | | | | |
| 1 barile (liquid barrel, bbl ^[16]) | 31.5 galo ¹ ⁄ ₂ hhd | 119,240 471 196 L | | | | | | | | | | | |
| 1 barile di petrolio (oil barrel, bo ^[16]) | 42 gal o ² ⁄ ₃ hhd | 158,987 294 928 L | | | | | | | | | | | |
| 1 hogshead (hhd) | 63 gal o 8 ²⁷ / ₆₄ ft ³ | 238,480 942 392 L | | | | | | | | | | | |

Volume secco

| Volume secco | | | | | | | | | | | |
|--------------------------------------|-----------------------|---------------------------|--|--|--|--|--|--|--|--|--|
| Unità | Divisioni | Equivalente SI | | | | | | | | | |
| 1 pinta (pt) | 33.60 in ³ | 550,610 5 cm ³ | | | | | | | | | |
| 1 quarto (qt) | 2 pt | 1,101 221 dm ³ | | | | | | | | | |
| 1 gallone (gal) | 4 qt | 4,404 884 dm ³ | | | | | | | | | |
| 1 peck (pk) | 2 gal | 8,809 768 dm ³ | | | | | | | | | |
| 1 staio ^[17] (bushel, bu) | 4 pk | 35,239 07 dm ³ | | | | | | | | | |
| 1 barile (<i>dry</i> barrel, bbl) | 7 056 in ³ | 115,627 1 dm ³ | | | | | | | | | |



Massa

| Тіро | Unità | Divisioni | Equivalenti Sl |
|-------------|--|--|-----------------------|
| | 1 grano (grain gr) | ¹ ⁄ ₇₀₀₀ lb | 64,798 91 mg |
| Avoirdupois | 1 dramma (dr) | 27¹¹/₃₂ gr (8,859 kt) | 1,771 845 195 312 5 g |
| | 1 oncia (oz o oz av) | 16 dr | 28,349 523 125 g |
| | <i>1 libbra (pound</i> , lb o lb av) | 16 oz | 453,592 37 g |
| | 1 quintale americano ^[20] (hundredweight, cwt) | 100 lb | 45,359 237 kg |
| | 1 quintale inglese ^[20] (long hundredweight) | 112 lb | 50,802 345 44 kg |
| | 1 ton (short ton) | 20 US cwt o 2000 lb | 907,184 74 kg |
| | 1 long ton | 20 long cwt o 2240 lb | 1 016,046 908 8 kg |



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Varie

$$1slug = \frac{1lbf}{ft/s^2} = \frac{1lbm \cdot g}{ft/s^2} = 32.17lbm = 14.593kg$$

$$g = 9.807 \frac{m}{s^2} = 9.807 \frac{\frac{1}{0.3048}ft}{s^2} = 32.175 \frac{ft}{s^2}$$

$$[\rho g] = \frac{lbf}{ft^3} = \frac{g \cdot 0.45359kg}{(.3048)^3m^3} = g \cdot 16.02 \frac{kg}{m^3}$$

$$1psi = 1 \frac{lbf}{in^2} = 1 \frac{lbm \cdot g}{ft^2/12^2} = 4632 \frac{lbm}{ft \cdot s^2} = 4632 \frac{.45359kg}{.3048m \cdot s^2} = 6895N$$

$$1BTU = 1kCal \frac{lbm \cdot R}{kg \cdot K} = 1kCal \frac{.45359}{1.8} = 4186.8 \cdot \frac{.45359}{1.8}J = 1055.1J$$

$$1hp = 550ft \cdot \frac{lbf}{s} = 550 \cdot 0.3048m \cdot 0.45359 \cdot \frac{kg}{s} \cdot g = 745.6W$$

$$xF = (x + 459.67)R = (x + 459.67)/1.8K = (x/1.8 + 255.37)K$$

$$xF = (x - 32)/1.8C = [(x - 32)/1.8 + 273.15]K$$



TSFC

Le unità di misura del consumo specifico (TSFC Thrust Specific Fuel Consumption) sono normalmente:

$$\begin{bmatrix} TSFC = \frac{\dot{m}_f}{F} \end{bmatrix} = \frac{lbm}{hr \cdot lbf} = \frac{lbm}{3600s \cdot 1lbm \cdot 32.17ft/s^2} = \frac{1}{115830} \frac{s}{ft}$$
$$= \frac{1}{115830} \frac{s}{0.3048m} = \frac{1}{34305} \frac{s}{m} = \frac{1}{34305} \frac{10^6 mg}{s \cdot kg \cdot m/s^2} = 28.325 \frac{mg}{s \cdot N}$$
$$\begin{bmatrix} TSFC = \frac{\dot{m}_f}{F} \end{bmatrix} = \frac{mg}{s \cdot N} = \frac{g}{s \cdot kN} = \frac{10^3 mg}{s \cdot kN} = \frac{10^{-6} kg}{s \cdot N}$$

Le unità di misura del calorifico del combustibile (fuel heating value) sono:

$$\begin{bmatrix} Q_R \end{bmatrix} = \frac{BTU}{lbm} = \frac{1055.1J}{lbm} = \frac{1055.1kg \cdot m^2}{lbm \cdot s^2} = \frac{\frac{1055.1}{0.3048^2}ft^2}{.45359 \cdot s^2} = 25038\frac{ft^2}{s^2} = 25038\frac{ft^2}{s^2} = 2326.1\frac{m^2}{s^2} = 2326.1\frac{J}{kg} = 2.3261\frac{kJ}{kg}$$



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Problem Fa2.34



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2.34 A scramjet combustor has a supersonic inlet condition and a choked exit. The combustor flow area increases linearly in the flow direction, as shown.

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The inlet and exit flow conditions are

$$M_1 = 3.0$$

 $p_1 = 1$ bar
 $T_1 = 1000$ K
 $A_1 = 1$ m²
 $M_2 = 1.0$
 $A_2 = 1.4$ m²
 $\gamma = 1.4$ R = 287 I/kg · K

The total heat release due to combustion, per unit flow rate in the duct, is initially *assumed* to be 15 MJ/kg. If we divide the combustor into three constant-area sections, with stepwise jumps in the duct area, we may apply Rayleigh flow principles to each segment, as shown. The heat release per segment is then 1/3 of the total heat release in the duct, i.e., 5,000 kJ/kg. As the exit condition of a segment needs to be matched to the inlet condition of the following segment, we propose to satisfy continuity equation at the boundary through an isentropic step area expansion, i.e., p_t , T_t remain the same and only the Mach number jumps isentropically through area expansion.

If we march from the inlet condition toward the exit with the assumed heat release rates, we calculate the exit Mach number M_2 . Since the exit flow is specified to be choked, then we need to adjust the total heat release in order to get a choked exit. Calculate the critical heat release in the above duct that leads to thermal choking of the flow.

| Sezione | 1 | 6 | | γ | 1.4 | | | | | | | | |
|------------|-----------|--------|--------|----------|--------|-------|---------|--------|-------|--------|-------|--------|-------|
| М | 3 | 1.2 | | R | 287 | J/kgK | ср | 1004.5 | J/kgK | | | | |
| Т | 1000 | | К | | | | | | | | | | |
| р | 1 | | bar | | | | | | | | | | |
| A | 1 | 1.4 | m/s | | | | | | | | | | |
| T1/Tt1 | 0.357 | | Tt1 | 2800 | К | | | | | | | | |
| Si usano 🛛 | 3 sezioni | quindi | 1-2 | 3-4 | 5-6 | | | | | | | | |
| | | A | 1 | 1.2 | 1.4 | | | | | | | | |
| O(kI/kg) | 500 | Ra | lso | Ra | lso | Ra | 0 | 600 | Ra | lso | Ra | lso | Ra |
| Sezione | 1 | 2 | 3 | 4 | 5 | 6 | Sezione | 1 | 2 | 3 | 4 | 5 | 6 |
| A | 1 | 1 | 1.2 | 1.2 | 1.4 | 1.4 | Α | 1 | 1 | 1.2 | 1.2 | 1.4 | 1.4 |
| М | 3 | 2.121 | 2.325 | 1.755 | 1.954 | 1.505 | Μ | 3 | 1.999 | 2.211 | 1.589 | 1.809 | 1.295 |
| T0/T0* | 0.654 | 0.770 | 0.736 | 0.847 | 0.803 | 0.908 | T0/T0* | 0.654 | 0.793 | 0.754 | 0.887 | 0.834 | 0.959 |
| Tt | 2800 | 3298 | 3298 | 3796 | 3796 | 4293 | Tt | 2800 | 3397 | 3397 | 3995 | 3995 | 4592 |
| A/A* | 4.23 | 1.870 | 2.24 | 1.392 | 1.624 | 1.179 | A/A* | 4.23 | 1.687 | 2.02 | 1.241 | 1.448 | 1.064 |
| Err | 0.305 | | | | | | Err | 0.095 | Q | 645.43 | | | |
| Q | 645.43 | Ra | lso | Ra | lso | Ra | Q | 639.21 | Ra | lso | Ra | lso | Ra |
| Sezione | 1 | 2 | 3 | 4 | 5 | 6 | Sezione | 1 | 2 | 3 | 4 | 5 | 6 |
| A | 1 | 1 | 1.2 | 1.2 | 1.4 | 1.4 | A | 1 | 1 | 1.2 | 1.2 | 1.4 | 1.4 |
| М | 3 | 1.948 | 2.1624 | 1.517 | 1.7491 | 1.185 | М | 3 | 1.955 | 2.1689 | 1.527 | 1.7571 | 1.202 |
| T0/T0* | 0.654 | 0.804 | 0.763 | 0.905 | 0.848 | 0.981 | T0/T0* | 0.654 | 0.803 | 0.762 | 0.903 | 0.846 | 0.978 |
| Tt | 2800 | 3443 | 3443 | 4085 | 4085 | 4728 | Tt | 2800 | 3436 | 3436 | 4073 | 4073 | 4709 |
| A/A* | 4.23 | 1.616 | 1.9396 | 1.188 | 1.3856 | 1.026 | A/A* | 4.23 | 1.626 | 1.9507 | 1.195 | 1.3937 | 1.031 |
| Err | -0.015 | Q | 639.21 | | | | | | | | | | |
| | | | | | | | | | | | | | |

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Problem E22 3/

At launch, the space shuttle main engine (SSME) has 1030 lbm/s of gas leaving the combustion chamber at $P_t = 3000$ psia and $T_t = 7350^{\circ}$ R. The exit area of the SSME nozzle is 77 times the throat area. If the flow through the nozzle is considered to be reversible and adiabatic (isentropic) with $Rg_c = 3800 \text{ ft}^2/(\text{s}^2 \cdot \text{°R})$ and $\gamma = 1.25$, find the area of the nozzle throat (in.²) and the exit Mach number. *Hint*: Use the mass flow parameter to get the throat area and Eq. (3.14) to get the exit Mach number.

$$\Psi(\gamma, M) = \frac{A^*}{A}\Psi^* = \gamma M \left(1 + \frac{\gamma - 1}{2}M^2\right)^{-\frac{(\gamma + 1)}{2(\gamma - 1)}} = \gamma M \psi^{-K}$$

con:

$$\psi(\gamma, M) = 1 + \frac{\gamma - 1}{2}M^2$$
 $K(\gamma) = \frac{(\gamma + 1)}{2(\gamma - 1)}$ $\Psi^* = \gamma \left(\frac{\gamma + 1}{2}\right)^{-\kappa}$



| | | | Tak | eoff | | | C | ruise | | |
|-------------|----------------------------|----------------|------------------|-------------------|-------------------|-------------|------|----------------|-------------------|--------------------------------------|
| Model no. | Manufacturer | Thrust, lbf | BR ^a | OPR ^b | Airflow, lbm/s | Alt, kft | Mach | Thrust, lbf | TSFC ^c | Application |
| CF 34-8 | General Electric | 14,500 | 5 | 28 | | | | | 0.68 | Bombardier CRJ700 Embraer 170/175 |
| CF6-50-C2 | General Electric | 52,500 | 4.31 | 30.4 | 1,476 | 35 | 0.80 | 11,555 | 0.630 | DC10-10, A300B, 747-200 |
| CF6-80-C2 | General Electric | 52,500 | 5.31 | 27.4 | 1,650 | 35 | 0.80 | 12,000 | 0.576 | 767-200, -300, -200ER |
| GE90-B4 | General Electric | 87,400 | 8.40 | 39.3 | 3,037 | 35 | 0.80 | 17,500 | | 777 |
| GEnx | General Electric | 53,000- | 10 | 42 | | | 0.85 | | | 787, 747-8 |
| | | 75,000 | | | | | | | | |
| JT8D-15A | Pratt & Whitney | 15,500 | 1.04 | 16.6 | 327 | 30 | 0.80 | 4,920 | 0.779 | 727, 737, DC9 |
| JT9D-59A | Pratt & Whitney | 53,000 | 4.90 | 24.5 | 1,639 | 35 | 0.85 | 11,950 | 0.646 | DC10-40, A300B, 747-200 |
| PW2037 | Pratt & Whitney | 38,250 | 6.00 | 27.6 | 1,210 | 35 | 0.85 | 6,500 | 0.582 | 757-200 |
| PW4052 | Pratt & Whitney | 52,000 | 5.00 | 27.5 | 1,700 | | | | | 767, A310-300 |
| PW4084 | Pratt & Whitney | 87,900 | 6.41 | 34.4 | 2,550 | 35 | 0.83 | | | 777 |
| CFM56-3C | CFM International | 23,500 | 6.00 | 22.6 | 655 | 35 | 0.80 | 5,540 | 0.648 | 737-300, -400, -500 |
| CFM56-5C | CFM International | 31,200 | 6.60 | 31.5 | 1,027 | 35 | 0.80 | 6,600 | 0.545 | A340 |
| AE 3007 | Rolls-Royce | 8,600 | 4.8 | 20 | | | | | | Embraer 37, Global Hawk UAV |
| RB211-524B | Rolls-Royce | 50,000 | 4.50 | 28.4 | 1,513 | 35 | 0.85 | 11,000 | 0.643 | L1011-200, 747-200 |
| RB211-535E | Rolls-Royce | 40,100 | 4.30 | 25.8 | 1,151 | 35 | 0.80 | 8,495 | 0.607 | 757-200 |
| RB211-882 | Rolls-Royce | 84,700 | 6.01 | 39.0 | 2,640 | 35 | 0.83 | 16,200 | 0.557 | 777 |
| Trent 900 | Rolls-Royce | 70,000- | 8.7- | | 2,655- | | | | | A380 |
| | | 76,500 | 8.5 | | 2,745 | | | | | |
| Trent 1000 | Rolls-Royce | 53,000- | 10 - 11 | | 2,400- | | | | | 787 |
| | | 75,000 | | | 2,670 | | | | | |
| V2528-D5 | International Aero Engines | 28,000 | 4.70 | 30.5 | 825 | 35 | 0.80 | 5,773 | 0.574 | MD-90 |
| ALF502R-5 | Honeywell | 6,970 | 5.70 | 12.2 | | 25 | 0.70 | 2,250 | 0.720 | BAe 146-200, -200 |
| TFE731-5 | Honeywell | 4,500 | 3.34 | 14.4 | 140 | 40 | 0.80 | 986 | 0.771 | BAe 125-800 |
| PW300 | Pratt & Whitney Canada | 4,750 | 4.50 | 23.0 | 180 | 40 | 0.80 | 1,113 | 0.675 | BAe 1000 |
| FJ44 | Williams Rolls | 1,900 | 3.28 | 12.8 | 63.3 | 30 | 0.70 | 600 | 0.750 | |
| Olympus 593 | Rolls-Royce/SNECMA | 38,000 | 0 | 11.3 ^d | 410 | 53 | 2.00 | 10,030 | 1.190 | Concorde |
| GP7270 | Engine Alliance | 70,000 | 8.7 ^d | 45.6 ^e | | 35 | 0.85 | 12,633 | | A380 |

^aBR = bypass ratio. ^bOPR = overall pressure ratio. ^cTSFC = thrust specific fuel consumption. ^dAt cruise. ^emax climb. (Sources: Manufacturers' literature).



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Some data

| | | | inperature/pressure | uata ioi some eng | | |
|---|--|---------------------------------|---------------------------------------|------------------------------------|---------------------------------------|--|
| Temperature and pressure | Pegasus turbofan, separate exhaust | J57 turbojet w/AB exhaust | JT3D turbofan, separate exhaust | JT8D turbofan, mixed exhaust | JT9D turbofan, separate exhaust | F100-PW-100 turbofan, mixed w/AB exhau |
| $\overline{P_{t2}}$, psia | 14.7 | 14.7 | 14.7 | 14.7 | 14.7 | 13.1 |
| T_{t2} , °F | 59 | 59 | 59 | 59 | 59 | 59 |
| $P_{t2.5}$, psia | 36.1 | 54 | 63 | 60 | 32.1 | 39.3 |
| $T_{t2.5}, {}^{\circ}\mathrm{F}$ | 242 | 330 | 360 | 355 | 210 | 297 |
| P_{t13} , psia | 36.5 | | 26 | 28 | 22.6 | 39.3 |
| T_{t13} , °F | 257 | | 170 | 190 | 130 | 297 |
| P_{t3} , psia | 216.9 | 167 | 200 | 233 | 316 | 316 |
| T_{t3} , °F | 708 | 660 | 715 | 800 | 880 | 1,014 |
| P_{t4} , psia | | 158 | 190 | 220 | 302 | 304 |
| T_{t4} , °F | 1,028 | 1,570 | 1,600 | 1,720 | 1,970 | 2,566 |
| P_{t5} or P_{t6} , psia | 29.3 | 36 | | 2 | 20.9 | 38.0 |
| T_{t5} or T_{t6} , $^{\circ}\mathrm{F}$ | 510 | 1,013 | | | 850 | 1,368 |
| P_{t16} , psia | | | | | | 36.8 |
| T_{t16} , °F | | | | | | 303 |
| P_{t6A} , psia | | | | 29 | | 37.5 |
| T_{t6A} , °F | | | | 890 | | 960 |
| P_{t7} , psia | | 31.9 | 28 | 29 | 20.9 | 33.8 |
| $T_{t7}, ^{\circ}\mathrm{F}$ | | 2,540 | 890 | 890 | 850 | 3,204 |
| P_{t17} , psia | 36.5 | | 26 | | 22.4 | |
| T_{t17} , °F | 257 | | 170 | | 130 | |
| Bypass ratio α | 1.4 | 0 | 1.36 | 1.1 | 5.0 | 0.69 |
| Thrust, lbf | 21,500 | 16,000 | 18,000 | 14,000 | 43,500 | 23,700 |
| Airflow, lbm/s | 444 | 167 | 460 | 315 | 1,495 | 224 |

Table B.4 Temperature/pressure data for some engines



II J57-JT3C è stato usato su: B-52, F-100, F-4 Phantom.



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Problem 3.1

3.1 The total pressures and temperatures of the gas in an afterburning turbojet engine are shown (J57 "B" from Pratt & Whitney, 1988). The mass flow rates for the air and fuel are also indicated at two engine settings, the Maximum Power and the Military Power. Use the numbers specified in this engine to calculate

- (a) the fuel-to-air ratio *f* in the primary burner and the afterburner, at both power settings
- (b) the low- and high-pressure spool compressor pressure ratios and the turbine pressure ratio (note that these remain constant with the two power settings)
- (c) the exhaust velocity V_9 for both power settings by assuming the specified thrust is based on the nozzle gross thrust (because of sea level static) and *neglecting any pressure thrust* at the nozzle exit
- (d) the thermal efficiency of this engine for both power settings (at the sea level static operation),





3.1 The total pressures and temperatures of the gas in an afterburning turbojet engine are shown (J57 "B" from Pratt & Whitney, 1988). The mass flow rates for the air and fuel are also indicated at two engine settings, the Maximum Power and the Military Power. Use the numbers specified in this engine to calculate

> (a) the fuel-to-air ratio f in the primary burner and the afterburner, at both power settings



TurboJet con e senza PB

286.857

- (b) the low- and high-pressure spool compressor pressure ratios and the turbine pressure ratio (note that these remain constant with the two power settings)
- (c) the exhaust velocity V_9 for both power settings by assuming the specified thrust is based on the nozzle gross thrust (because of sea level static) and neglecting any pressure thrust at the nozzle exit
- (d) the thermal efficiency of this engine for both power settings (at the sea level static operation), assuming the fuel heating value is 18,600 BTU/lbm and $c_p = 0.24$ BTU/lbm · °R. Explain the lower thermal efficiency of the Maximum power setting
- (e) the thrust specific fuel consumption in lbm/h/lbf in both power settings
- (f) the Carnot efficiency of a corresponding engine, i.e., operating at the same temperature limits, in both settings
- (g) the comparison of percent thrust increase to percent fuel flow rate increase when we turn the afterburner on
- (h) why don't we get proportional thrust increase with fuel flow increase (when it is introduced in the afterburner), i.e., doubling the fuel flow in the engine (through afterburner use) does not double the thrust

Turbo Jet By TomLevel 4 2 3 5 7 4 9 dcb t diff CC Tur AB No comp 1243 J/kg. 1004 1152 1.4 1.33 1.3 0.96 10 0.95 0.98 0.97 η, e _{c,t} 0.9 0.99 0.9 0.99 1750 2250 2 po/p9 42800 kJ/kgK 1 QR 250 K 101,300 Pa p0 η_m 0.99 0.23077 0.28571 0.24812

285.835



Cp

γ

 π

Τt

M0

T0

k

R

JT3D-3B è stato usato su: B707 e DC8.



Problem 3.2



JT3D-3B Turbofan Internal pressures and temperatures



3.2 The total pressures and temperatures of the gas are specified for a turbofan engine with separate exhaust streams (JT3D-3B from Pratt & Whitney, 1974). The mass flow rates in the engine core (or primary) and the engine fan are also specified for the sea level static operation. Calculate

- (a) the engine bypass ratio α defined as the ratio of fan-to-core flow rate
- (b) from the total temperature rise across the burner, estimate the fuel-to-air ratio and the fuel flow rate in lbm/h, assuming the fuel heating value is $Q_R \sim 18,600$ BTU/ lbm and the specific heat at constant pressure is 0.24 and 0.26 BTU/lbm \cdot °R at the entrance and exit of the burner, respectively
- (c) the engine static thrust based on the exhaust velocities and the mass flow rates *assuming perfectly expanded nozzles* and compare your answer to the specified thrust of 18,000 lbs
- (d) the engine thermal efficiency $\eta_{\rm th}$

- (e) the thermal efficiency of this engine compared to the afterburning turbojet of Problem 1. Explain the major contributors to the differences in η_{th} in these two engines
- (f) the engine thrust specific fuel consumption in lbm/h/lbf
- (g) the nondimensional engine specific thrust
- (h) the Carnot efficiency corresponding to this engine
- (i) the engine overall pressure ratio p_{t3} / p_{t2}
- (j) fan nozzle exit Mach number [use $T_t = T + V^2/2c_p$ to calculate local static temperature at the nozzle exit, then local speed of sound $a = (\gamma RT)^{1/2}$]

JT3D-3B Turbofan Internal pressures and temperatures



Problem 3.3

JT8D è stato usato su: B727, DC9 e MD80.

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Problem 3.3

3.3 A mixed exhaust turbofan engine (JT8D from Pratt and Whitney, 1974) is described by its internal pressures and temperature, as well as air mass flow rates and the mixed jet (exhaust) velocity. Let us examine a few parameters for this engine, for a ballpark approximation.

- (a) Estimate the fuel flow rate from the total temperature rise across the burner assuming the fuel heating value is ~18,600 BTU/lbm and the specific heat at constant pressure is 0.24 and 0.26 BTU/lbm · °R at the entrance and exit of the burner, respectively
- (b) Calculate the momentum thrust at the exhaust nozzle and compare it to the specified thrust of 14,000 lbs
- (c) Estimate the thermal efficiency of this engine and compare it to Problems 3.1 and 3.2 as well as a Carnot cycle operating between the temperature extremes of this engine. Explain the differences
- (d) Estimate the specific fuel consumption for this engine in lbm/h/lbf
- (e) The overall pressure ratio (of the fan-compressor section) p_{t3}/p_{t2}

- (f) What is the bypass ratio α for this engine at takeoff
- (g) What is the Carnot efficiency corresponding to this engine
- (h) Estimate nozzle exit Mach number [look at part (j) in Problem 3.2]
- (i) What is the low-pressure compressor (LPC) pressure ratio $p_{t2.5}/p_{t2}$
- (j) What is the high-pressure compressor (HPC) pressure ratio p_{t3} / $p_{t2.5}$





JT9D è stato usato su: B747, A310 e 767.



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Problem 3.4





3.4 A large bypass ratio turbofan engine (JT9D engine from Pratt and Whitney, 1974) is described by its fan and core engine gas flow properties.

- (a) What is the overall pressure ratio (OPR) of this engine
- (b) Estimate the fan gross thrust $F_{g,fan}$ in lbf
- (c) Estimate the fuel-to-air ratio based on the energy balance across the burner, assuming the fuel heating value is ~18,600 BTU/lbm and the specific heat at constant pressure is 0.24 and 0.26 BTU/lbm \cdot °R at the entrance and exit of the burner, respectively
- (d) Calculate the core gross thrust and compare the sum of the fan and the core thrusts to the specified engine thrust of 43,500 lbf
- (e) Calculate the engine thermal efficiency and compare it to Problems 3.1–3.3. Explain the differences
- (f) Estimate the thrust-specific fuel consumption (TSFC), in lbm/h/lbf
- (g) What is the bypass ratio of this turbofan engine

- (h) What is the Carnot efficiency η_{Carnot} corresponding to this engine
- (i) What is the LPC pressure ratio $p_{t2.5} / p_{t2}$
- (j) What is the HPC pressure ratio $p_{t3} / p_{t2.5}$
- (k) Estimate the fan nozzle exit Mach number [see part (j) in Problem 3.2]
- (I) Estimate the primary nozzle exit Mach number





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Problem 3.4

Valutare inoltre il lavoro nei vari stadi del compressore, nella turbina e il calore scambiato nella camera di combustione.



TurboFan

| JT9d By To | om | | | | | | | 113 | 1.0 |
|---------------------|---------|------|-------|---------|--------|----------|--------|-------|--------------------------|
| | 2 | 3 | 4 | 5 | 9 | 13 | 19 | | |
| | diff | comp | CC | Tur | No | Fan | No FAn | dfc]] | $\sum_{i=1}^{n} t_i n_i$ |
| с _р | 1004 | | | 1057 | | | | 3 | 4 |
| γ | 1.4 | | | 1.35 | | | | | |
| π | 1 | 21.5 | 0.955 | | 0.98 | 1.53 | 0.99 | | |
| η, e _{c,t} | | 0.92 | 0.95 | 0.9 | | 0.96 | | | |
| Tt | | | | 1349.8 | | | | | |
| M0 | 0 | | | | QR | 42800 | kJ/kgK | | |
| то | 288 | К | p0 | 101,300 | Ра | η_m | 0.98 | | |
| alpha | 5.053 | | | | | | | | |
| k | 0.28571 | | | 0.25926 | | | | | |
| R | 286.857 | | | 274.037 | kJ/kgK | | | | |
| a0 | 340.1 | m/s | V0 | 0.0 | m/s | | | | |



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TurboProp

| Turbo Pro | p FaE4.38 | | | | | | | 2 | 4.55 |
|---------------------|-----------|------|------|---------|--------|-------------|--------|-------------|----------|
| | 2 | 3 | 4 | 4.5 | 5 | 9 | 0/ | $\sqrt{34}$ | 1^{9} |
| | diff | comp | CC | Tur | Tur | No | Prop d | i cjbił | nti [nj] |
| с _р | 1004 | | | 1152 | J/kgs | | | | |
| γ | 1.4 | | | 1.33 | | | | | |
| π | 0.99 | 35 | 0.96 | | | | | | |
| η, e _{c,t} | | 0.92 | 0.99 | 0.8 | 0.859 | 0.95 | 0.85 | | |
| Tt | | | | 1650 | | | | | |
| M0 | 0.82 | | | | QR | 42000 | kJ/kgK | | |
| то | 258 | К | p0 | 30,000 | Ра | η_m H | 0.99 | | |
| alpha | 0.75 | m0 | 50 | kg/s | | η_m L | 0.99 | | |
| k | 0.28571 | | | 0.24812 | | η_{gb} | 0.995 | | |
| R | 286.857 | | | 285.835 | kJ/kgK | | | | |
| a0 | 321.9 | m/s | V0 | 263.9 | m/s | | | | |



Prese d'aria ed ugelli

MA4.3 The inlet for a high-bypass-ratio turbofan engine has an area A_1 of 6.0 m² and is designed to have an inlet Mach number M_1 of 0.6. Determine the additive drag at the flight conditions of sea-level static test and Mach number of 0.8 at 12-km altitude.

6.3 Consider a subsonic inlet at a flight cruise Mach number of 0.8. The captured streamtube undergoes a prediffusion external to the inlet lip, with an area ratio $A_0/A_1 = 0.92$, as shown. Calculate

- (a) C_p (i.e., the pressure coefficient) at the stagnation point
- (**b**) inlet lip Mach number M_1
- (c) lip contraction ratio A_1/A_{th} for a throat Mach number $M_{th} = 0.75$ (assume $p_{t,th}/p_{t1} = 1$)
- (d) the diffuser area ratio $A_2/A_{\rm th}$ if $M_2 = 0.5$ and $p_{\rm t2}/p_{\rm t,th} = 0.98$
- (e) the nondimensional inlet additive drag $D_{\rm add}/p_0A_1$.

Stagnation point A_0 A_1 A_0 A_1 A_1 A_0 A_1 A_2 M_1 Propulsione Aerospaziale – ES PA - astarita @unina.it

6.17 A normal-shock inlet is operating in a supercritical mode, as shown. Flight Mach number is $M_0 = 1:6$. The inlet capture area ratio $A_0 / A_1 = 0:90$ and the diffuser area ratio $A_2/A_1 = 2$. Calculate



(**b**) inlet total pressure recovery π_d , i.e., p_{t2}/p_{t0}



Prese d'aria ed ugelli

6.18 An isentropic convergent-divergent supersonic inlet is designed for $M_D = 1.6$. Calculate the inlet's

- (a) area contraction ratio $A_1/A_{\rm th}$
- (b) subsonic Mach number where the throat first chokes
- (c) percent spillage at $M_0 = 0.7$
- (d) percent spillage at $M_0 = 1.6$ (in the unstarted mode)
- (e) overspeed Mach number to start this inlet, $M_{\text{overspeed}}$
- (f) throat Mach number after the inlet was started, with still $M_{\text{overspeed}}$ as the flight Mach number

6.23 A Kantrowitz–Donaldson inlet is designed for $M_{\rm D} = 1.7$. Calculate

- (a) the inlet contraction ratio $A_1/A_{\rm th}$
- (b) the throat Mach number after the inlet self started
- (c) the total pressure recovery with the best backpressure.



6.43 A convergent nozzle experiences π_{cn} of 0.98, the gas ratio of specific heats $\gamma = 1.30$, and the gas constant is $R = 291 \text{ J/kg} \cdot \text{K}$. First, calculate the minimum nozzle pressure ratio that will choke the expanding nozzle, i.e., NPR_{crit}. This nozzle operates, however, at a higher NPR than the critical, namely, NPR = 4. 2 and with an inlet stagnation temperature of $T_{t7} = 939 \text{ K}$. Assuming this nozzle operates in $p_0 = 100 \text{ kPa}$ ambient static pressure, calculate

- (a) the exit static pressure and temperature p_9 and T_9 , respectively
- (b) the actual exit velocity V_9 in m/s
- (c) nozzle adiabatic efficiency η_n
- (d) the ideal exit velocity V_{9s} in m/s
- (e) percentage gross thrust gain, had we used a convergent-divergent nozzle with perfect expansion
- (f) nozzle discharge coefficient C_{D8}
- (g) draw a qualitative wave pattern in the exhaust plume

6.44 A convergent-divergent nozzle has a conical exhaust shape with the half-cone angle of $\alpha = 25^{\circ}$. Calculate the divergence loss C_A for this nozzle due to nonaxial exhaust flow. Assuming the same (half) divergence angle of 25°, but in a 2D rectangular nozzle, calculate the flow angularity loss and compare it to the conical case.



Problem MA2.6

One method of reducing an aircarft's landing distance is through the use of thrust reversers. Consider the turbofan engine in Fig. P2.5 with thrust reverser of the bypass airstream. It is given that 1500 lbm/s of air at 60°F and 14.7 psia enters the engine at a velocity of 450 ft/s and that 1250 lbm/s of bypass air leaves the engine at 60 deg to the horizontal, velocity of 890 ft/s, and pressure of 14.7 psia. The remaining 250 lbm/s leaves the engine core at a velocity of 1200 ft/s and pressure of 14.7 psia. Determine the force on the strut F_x . Assume the outside of the engine sees a pressure of 14.7 psia.



Camera di combustione

7.4 Write the chemical reaction for the complete combustion of JP-4 and air. JP-4 has the formula $CH_{1.93}$. Also, calculate the stoichiometric fuel-to-air ratio for this blended jet fuel.

7.5 Calculate the lower and higher heating values of octane, C_8H_{18} , in the stoichiometric chemical reaction *with oxygen* at a reference temperature of 298.16 K and the pressure of 1 bar.

$$C_8H_{18(g)} + 12.5O_{2(g)} \rightarrow 8CO_{2(g)} + 9H_2O$$

7.9 One mole of octane is burned with 120% theoretical air. Assuming that the octane and air enter the combustion chamber at 25°C and the excess oxygen and nitrogen in the reaction will not dissociate, calculate

- (a) the fuel–air ratio
- (b) the equivalence ratio ϕ
- (c) the adiabatic flame temperature $T_{\rm af}$

Assume

$$\bar{c}_{p_{CO_2}} = 61.9 \text{ kJ/kmol} \cdot \text{K}, \ \bar{c}_{p_{O_2}} = 37.8 \text{ kJ/kmol} \cdot \text{K}$$

 $\bar{c}_{p_{N_2}} = 33.6 \text{ kJ/kmol} \cdot \text{K}, \ \bar{c}_{p_{H_2O}} = 52.3 \text{ J/kmol} \cdot \text{K}$

7.10 One mole of oxygen, $O_{2(g)}$, is heated to 4000 K at the pressure of p_m . A fraction of the oxygen dissociates to oxygen atoms according to

$$xO_2 \rightarrow 2xO$$

Assuming a state of equilibrium is reached in the mixture, calculate

- (a) mole fraction of O_2 at equilibrium when p_m is 1 atm.
- (b) mole fraction of O_2 at equilibrium when p_m is 10 atm.

Assume the equilibrium constant for the reaction

$$O_2 \leftrightarrow 2O$$

is $K_p = 2.19$ atm at the temperature of 4000 K. Explain the effect of pressure on dissociation.



Consideriamo ora la reazione:

$$H_2 + \frac{1}{2}O_2 \leftrightarrow n_{H_2O}H_2O + n_{H_2}H_2 + n_{O_2}O_2 + n_{OH}OH + n_OO + n_HH$$

per equilibrare questa reazione si procede inizialmente ad equilibrare le singole specie ottenendo:



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Si devono quindi analizzare le sotto reazioni:

| $\bullet \frac{1}{2}$ | 0 ₂ ← | → 0 | | \rightarrow | K _p | $b_1 = \frac{1}{p}$ | $\frac{p_0}{1/2} =$ | $=\frac{\chi_0}{\chi_{02}^{1/2}}p_m^{1/2}$ |
|-----------------------|---------------------|--------------------|---------------------|---------------|----------------|------------------------|-------------------------------|---|
| $\bullet \frac{1}{2}$ | H ₂ ← | → H | | \rightarrow | K _µ | $b_{p2} = \frac{1}{p}$ | $\frac{p_H}{1/2} = H_2$ | $=\frac{\chi_{H}}{\chi_{H_{2}}^{1/2}}p_{m}^{1/2}$ |
| $\bullet \frac{1}{2}$ | H ₂ + | $\frac{1}{2}0$ | ₂ ↔ OH | | \rightarrow | | К _{р3} | $=\frac{p_{OH}}{p_{\rm H_2}^{1/2}p_{\rm O_2}^{1/2}}=\frac{\chi_{OH}}{\chi_{\rm H_2}^{1/2}\chi_{\rm O_2}^{1/2}}$ |
| • F | $H_2 + \frac{1}{2}$ | $\frac{1}{2}0_{2}$ | ↔ H ₂ O | | \rightarrow | | <i>K</i> _{<i>p</i>4} | $=\frac{p_{\rm H_2O}}{p_{\rm H_2}p_{\rm O_2}^{1/2}}=\frac{\chi_{\rm H_2O}}{\chi_{\rm H_2}\chi_{\rm O_2}^{1/2}}p_m^{-1/2}$ |
| % | | 1 | 2 | 3 | 4 | 5 | 6 | |
| Spe | ={ 'H2 | 20' | ,'H2', | '02', | 'ОН', | '0',' | 'Н'} | • " |
| Rea | =[| 0 | 0 | -0.5 | 0 | 1 | 0; | |
| | | 0 | -0.5 | 0 | 0 | 0 | 1; | |
| | | 0 | -0.5 | -0.5 | 1 | 0 | 0; | |
| | | 1 | -1 | -0.5 | 0 | 0 | 0] | • • |
| for | i=1 | :Nr | | | | | | |
| | ind | =Rea | a(i,:) [,] | ~=0; | | | | |
| | R(N | o+i) |)=K(i) | -prod | (chi(| ind). | ^Rea | a(i,ind))*p^sum(Rea(i,ind)); |
| end | - | - | | • | - | - | | |



```
function R=Reazione (n,p,K,Rea,Bil)
R=0*n;
n=abs(n);
%Bilancio stechiometrico
Nb=size(Bil,1);
for i=1:Nb
        R(i)=sum(Bil(i,1:end-1).*n)-Bil(i,end);
end
% costanti
chi=n/sum(n);
Nr=size(Rea,1);
for i=1:Nr
        ind=Rea(i,:)~=0;
        R(Nb+i)=K(i)-prod(chi(ind).^Rea(i,ind))*p^sum(Rea(i,ind));
end
```



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| % | Н2С |)2 | | | | | | | | |
|----------|---------------------|------------------|--------|--------------------------------------|---------------|--------------------------------|--------------------------|----------------------|-----------------------------|---------|
| % | 1 | 2 | 3 | 4 | 5 | 6 | | | | |
| Spe={ 'H | 20', | 'H2', | '02',' | ОН',' | 0',' | Н'}; | | | | |
| Rea=[| 0 | 0 | -0.5 | 0 | 1 | 0; | | | | |
| | 0 | -0.5 | 0 | 0 | 0 | 1; | | | | |
| | 0 | -0.5 | -0.5 | 1 | 0 | 0; | | | | |
| | 1 | -1 | -0.5 | 0 | 0 | 0]; | | | | |
| Bil=[| 2 | 2 | 0 | 1 | 0 | 1 | 2*1/1.0 | 0794; | | |
| | 1 | 0 | 2 | 1 | 1 | 0 | 1*16/15 | .9994]; | | |
| n= [| 4 | .1 | 0.1 | .1 | .1 | .1]; | | | | |
| p=20*1. | 013; | | | | | | | | | |
| K=[0.48 | 9778 | 8819 0 | .58748 | 39353 | 1.44 | 54392 | 771 5.15 | 2286446 | 5]; | |
| options | = 0 | optims | et('Di | splay | ','o | off', | 'Tolx',1 | e-18,'T | <code>TolFun',</code> | le-18); |
| n2=fsol | ve(@ | Reazi | one, r | n,opti | ons | ,р,К | ,Rea,Bil |); | | |
| fprintf | (' <mark>c</mark> s | si= ') | ;fprir | ntf(<mark>'%</mark> | .3g | ',n2, | /sum(n2) |); | | |
| | Т(К) | $\frac{1}{2}O_2$ | ↔ 0 | $\frac{1}{2}H_2 \leftrightarrow H_2$ | $\frac{1}{2}$ | $\frac{1}{2}H_2 + \frac{1}{2}$ | $0_2 \leftrightarrow 0H$ | $H_2 + \frac{1}{2}G$ | $D_2 \leftrightarrow H_2 O$ | |
| | 3500 | -0.3 | 310 | -0.231 | | 0. | 160 | 0. | 712 | |

0.233

0.238

Logaritmo in base 10 delle cosanti d'equilibrio Kp



4000

0.170

0.201

This appendix (<u>ceaThermoBuild</u>) explains the format for data contained in the file thermo.inp (app. D). Equations (1) to (3) are repeated here for convenience:

$$\begin{aligned} \frac{\bar{c}_p}{\bar{R}} &= a_1 T^{-2} + a_2 T^{-1} + a_3 + a_4 T + a_5 T^2 + a_6 T^3 + a_7 T^4 \\ \frac{\bar{h}}{\bar{R}T} &= -a_1 T^{-2} + a_2 \frac{\ln T}{T} + a_3 + a_4 \frac{T}{2} + a_5 \frac{T^2}{3} + a_6 \frac{T^3}{4} + a_7 \frac{T^4}{5} + b_1 \frac{1}{T} \\ \frac{\bar{S}}{\bar{R}} &= -a_1 \frac{T^{-2}}{2} - a_2 T^{-1} + a_3 \ln T + a_4 T + a_5 \frac{T^2}{2} + a_6 \frac{T^3}{3} + a_7 \frac{T^4}{4} + b_2 \end{aligned}$$

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Si dimostra che per una generica reazione chimica:

$$\ln K_p = \sum \left(\frac{\bar{h}}{\bar{R}T} - \frac{\bar{S}}{\bar{R}}\right)^{-r}$$

dove *r* è il coefficiente stechiometrico della reazione. Per esempio:

•
$$\frac{1}{2}O_2 \leftrightarrow 0 \rightarrow K_{p1} = \frac{p_0}{p_{0_2}^{1/2}} = \frac{\chi_0}{\chi_{0_2}^{1/2}} p_m^{1/2}$$

 $\ln K_{p1} = \left(\frac{\bar{h}}{\bar{R}T} - \frac{\bar{S}}{\bar{R}}\right)_{O_2}^{\frac{1}{2}} + \left(\frac{\bar{h}}{\bar{R}T} - \frac{\bar{S}}{\bar{R}}\right)_{O}^{-1}$



| Record | Contents | FORTRAN format | Columns |
|--------|--|-------------------|----------|
| 1 | Species name or formula | A16 | 1 to 16 |
| | Comments and data sources | A62 | 19 to 80 |
| 2 | Number of T intervals | I2 | 1 to 2 |
| | Reference date code | A6 | 4 to 9 |
| | Chemical formula—symbols (all capitals) and numbers | 5(A2, F6.2) | 11 to 50 |
| | Zero for gas; nonzero for condensed ^a | I2 | 51 to 52 |
| | Molecular weight | F13.7 | 53 to 65 |
| | Heat of formation at 298.15 K, J/mol | F15.5 | 66 to 80 |
| 3 | Temperature range | 2F11.3 | 1 to 22 |
| | Number of coefficients for $C_p^o(T)/R$ (always seven) | I1 | 23 |
| | T exponents in empirical equation for $C_p^{o}(T)/R$ | 8F5.1 | 24 to 63 |
| | [always $-2, -1, 0, 1, 2, 3, 4$; see eq. (1)] | | |
| | $H^{o}(298.15) - H^{o}(0)$ J/mol, if available | F15.3 | 66 to 80 |
| 4 | First five coefficients for $C_p^o(T)/R$, eq. (1) | 5D16.9 | 1 to 80 |
| 5 | Last two coefficients for $C_p^o(T)/R$, eq. (1) | 2D16.9 | 1 to 32 |
| | Integration constants b_1 and b_2 , eqs. (2) and (3) | 2D16.9 | 49 to 80 |
| _ | Repeat 3, 4, and 5 for each interval | | |

Camera di combustione

La funzione (LeggiFileCea.m) risolve il problema della lettura dei file di testo restituendo una struttura con i seguenti campi:

```
NInt: 2
WM: 18.0153
DH0: -241826
TInt: [2×2 double]
Esp: [2×7 double]
DH1: [2×2 double]
a: [2×7 double]
b: [2×2 double]
           123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678901234567890123456789012345678900123456789001234567890012345678900000
                                                                      40
                        10
                                       20
                                                       30
                                                                                     50
                                                                                                    60
                                                                                                                   70
                                                                                                                                   80
          TiN(cr)
                                     Chase,1998 pp1612-4.
    1
            2 j 6/68 TI 1.00N 1.00
                                                                                0.00 1
     2
                                                      0.00
                                                                    0.00
                                                                                                 61.87374
                                                                                                                   -337648.800
     3
                                 800.0007 -2.0 -1.0 0.0 1.0 2.0 3.0 4.0 0.0
                 200.000
                                                                                                                        5487.000
     4
           -5.479117220D+05 9.328691110D+03-6.386263890D+01 2.429925456D-01-4.304234520D-04
     5
            3.792645100D-07-1.317412256D-10
                                                                                   -8.424256140D+04 3.392988560D+02
     6
                 800.000
                                3220.0007 -2.0 -1.0 0.0 1.0 2.0 3.0 4.0 0.0
                                                                                                                        5487.000
     7
           -3.656247060D+05 1.265730431D+03 3.831711190D+00 1.632900455D-03-1.062786626D-07
     8
            1.310931390D-11-5.770548410D-16
                                                                                    -5.027654400D+04-1.652632899D+01
     9
          TiN(L)
                                      Chase, 1998 pp1612-4.
                                                        0.00
                                                                    0.00
    10
            1 j 6/68 TI
                                1.00N
                                            1.00
                                                                                0.00 2
                                                                                                 61.87374
                                                                                                                   -337648.800
               3220.000
                                6000.0007 -2.0 -1.0 0.0 1.0
    11
                                                                             2.0 3.0
                                                                                              4.0 0.0
                                                                                                                        5487.000
            0.0000000D+00 0.0000000D+00 7.548249987D+00 0.0000000D+00 0.0000000D+00
    12
                                                                                   -3.626039860D+04-3.958296649D+01
     13
            0.0000000D+00 0.0000000D+00
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```

Camera di combustione GLENN RESEARCH CENTER +Visit Glenn +Visit NASA Chemical Canilip with Applications + CHEMICAL EQUILIBRIUM RELATED TOPICS THERMO BUILD +Home Written by Patrick Chan (NASA Summer Intern 2001 Duke University sophomore), ThermoBuild is an interactive **Related Topics** tool which uses the NASA Glenn thermodynamic database to select species and to obtain: 1. Tables of thermodynamic properties for a user-supplied temperature schedule. + ONLINE CEA! Data subsets for use in CEA, SUBEQ or any other computer program. + CAP To generate a data subset, click here. + PAC Click on symbols for atoms contained in desired compounds. 2 13 14 16 17 15 н D He 1 IIIA IVA WA MA MIA 3A 4A 5A 6A 7A \sim а a. 9 10 s 6 a Allow ions: В Li Be С N 0 F Ne 2 $\overline{}$ 45 Propulsione Aerospaziale - ES PA - astarita@unina.it

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ThermoBuild (page 2)

Jump to bottom of page

Instructions: To generate the desired thermodynamic data, please choose from the following species (Air is provided as a convenience):

| <u>Choose</u> | <u>Species Name</u> | <u>Beginning Temperature</u> (K) | End Temperature (K) |
|---------------|---------------------|----------------------------------|---------------------|
| | H | 200.000 | 20000.000 |
| | HO2 | 200.000 | 6000.000 |
| | H2 | 200.000 | 20000.000 |
| Ø | H2O | 200.000 | 6000.000 |
| | H2O2 | 200.000 | 6000.000 |
| | 0 | 200.000 | 20000.000 |
| | OH | 200.000 | 20000.000 |
| | 02 | 200.000 | 20000.000 |
| | 03 | 200.000 | 6000.000 |
| | H2O(cr) | 200.000 | 273.150 |
| | H2O(L) | 273.150 | 600.000 |
| | Air | 200.000 | 6000.000 |
| | | | |



ThermoBuild

(page 3)

| Energy Units: | | | |
|---|---|-----------------------|----|
| Joules | | Calories | |
| Temperature Sche Each row used must | dule (Kelvin) be complete. Interv | als may be zero (0.0) |). |



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Ranges:

| 298.150 | 798.150 | 1298.150 | 1798.150 | 2298.150 | 2798.150 |
|----------|----------|----------|----------|----------|----------|
| 3298.150 | 3798.150 | 4000.000 | | | |

NOTE: Thermodynamic properties calculated for temperatures outside the range of the fitted data may have large errors. This program allows calculations only for temperatures within 20% above or below the fitted temperature range.

COEFFICIENTS FOR FITTED THERMODYNAMIC FUNCTIONS

H20 Hf:Cox,1989. Woolley,1987. TRC(10/88) tuv25. 2 g 8/89 H 2.000 1.00 0.00 0.00 0.00 0 18.01528 -241826.000 200.000 1000.000 7 -2.0 -1.0 0.0 1.0 2.0 3.0 4.0 0.0 9904.092 -3.947960830E+04 5.755731020E+02 9.317826530E-01 7.222712860E-03-7.342557370E-06 4.955043490E-09-1.336933246E-12 0.00000000E+00-3.303974310E+04 1.724205775E+01 1000.000 6000.000 7 -2.0 -1.0 0.0 1.0 2.0 3.0 4.0 0.0 9904.092 1.034972096E+06-2.412698562E+03 4.646110780E+00 2.291998307E-03-6.836830480E-07 9.426468930E-11-4.822380530E-15 0.00000000E+00-1.384286509E+04-7.978148510E+00



-3.947960830E+04 5.755731020E+02 9.317826530E-01 7.222712860E-03-7.342557370E-06 4.955043490E-09-1.336933246E-12 0.00000000E+00-3.303974310E+04 1.724205775E+01 1000.000 6000.000 7 -2.0 -1.0 0.0 1.0 2.0 3.0 4.0 0.0 9904.092 1.034972096E+06-2.412698562E+03 4.646110780E+00 2.291998307E-03-6.836830480E-07 9.426468930E-11-4.822380530E-15 0.00000000E+00-1.384286509E+04-7.978148510E+00

THERMODYNAMIC FUNCTIONS CALCULATED FROM COEFFICIENTS FOR H20

| Ср | н-н298 | S | -(G-H298)/T | Н | delta Hf | log K |
|---------|---|---|---|---|--|--|
| J/mol-K | kJ/mol | J/mol-K | J/mol-K | kJ/mol | kJ/mol | |
| 0 | 0 004 | 0 | | 261 720 | 000 000 | |
| υ. | -9.904 | υ. | INFINITE | -201./30 | -230.922 | INFINITE |
| 33.588 | 0.000 | 188.829 | 188.829 | -241.826 | -241.826 | 40.0453 |
| 38.705 | 17.931 | 223.732 | 201.265 | -223.895 | -246.429 | 13.3235 |
| 45.043 | 38.880 | 243.985 | 214.035 | -202.946 | -249.447 | 7.0765 |
| 50.160 | 62.753 | 259.496 | 224.598 | -179.073 | -250.990 | 4.2768 |
| 53.698 | 88.775 | 272.247 | 233.618 | -153.051 | -251.655 | 2.6883 |
| 56.090 | 116.261 | 283.061 | 241.512 | -125.565 | -251.903 | 1.6657 |
| 57.731 | 144.740 | 292.421 | 248.536 | -97.086 | -252.031 | 0.9526 |
| 58.921 | 173.917 | 300.656 | 254.866 | -67.909 | -252.212 | 0.4270 |
| 59.325 | 185.852 | 303.718 | 257.255 | -55.974 | -252.323 | 0.2519 |
| | Cp J/mol-K 33.588 38.705 45.043 50.160 53.698 56.090 57.731 58.921 59.325 | Cp H-H298 J/mol-K kJ/mol 09.904 33.588 0.000 38.705 17.931 45.043 38.880 50.160 62.753 53.698 88.775 56.090 116.261 57.731 144.740 58.921 173.917 59.325 185.852 | CpH-H298SJ/mol-KkJ/molJ/mol-K09.9040.33.5880.000188.82938.70517.931223.73245.04338.880243.98550.16062.753259.49653.69888.775272.24756.090116.261283.06157.731144.740292.42158.921173.917300.65659.325185.852303.718 | CpH-H298S- (G-H298)/TJ/mol-KkJ/molJ/mol-KJ/mol-K09.9040.INFINITE33.5880.000188.829188.82938.70517.931223.732201.26545.04338.880243.985214.03550.16062.753259.496224.59853.69888.775272.247233.61856.090116.261283.061241.51257.731144.740292.421248.53658.921173.917300.656254.86659.325185.852303.718257.255 | CpH-H298S-(G-H298)/THJ/mol-KkJ/molJ/mol-KJ/mol-KkJ/mol09.9040.INFINITE-251.73033.5880.000188.829188.829-241.82638.70517.931223.732201.265-223.89545.04338.880243.985214.035-202.94650.16062.753259.496224.598-179.07353.69888.775272.247233.618-153.05156.090116.261283.061241.512-125.56557.731144.740292.421248.536-97.08658.921173.917300.656254.866-67.90959.325185.852303.718257.255-55.974 | CpH-H298S-(G-H298)/THdelta HfJ/mol-KkJ/molJ/mol-KJ/mol-KkJ/molkJ/mol09.9040.INFINITE-251.730-238.92233.5880.000188.829188.829-241.826-241.82638.70517.931223.732201.265-223.895-246.42945.04338.880243.985214.035-202.946-249.44750.16062.753259.496224.598-179.073-250.99053.69888.775272.247233.618-153.051-251.65556.090116.261283.061241.512-125.565-251.90357.731144.740292.421248.536-97.086-252.03158.921173.917300.656254.866-67.909-252.21259.325185.852303.718257.255-55.974-252.323 |



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Camera di combustione

```
function [cp_R H_RT S_R]=TermoCea(T,S)
% Con R =8314.5 J/kmole K
% cp=cp_R*R [J/kmole K]
% H*H_RT*R*T [J/kmole]
% S=S_R*R [J/kmole K]
% G=S_R*R*T [J/kmole]
%Verifica intervallo di temperature
if T<S.TInt(1,1) |T>S.TInt(:,:)
   error ('Temperture outside limits')
end
%Trova l'indice dell'intervallo di temperature
for i=1:S.NInt
   if T<S.TInt(i,2)</pre>
      ic=i;
      break;
   end
end
```



function [cp_R H_RT S_R]=TermoCea(T,S)
•
$$\frac{\bar{c}_p}{\bar{R}} = a_1 T^{-2} + a_2 T^{-1} + a_3 + a_4 T + a_5 T^2 + a_6 T^3 + a_7 T^4$$

cp_R=sum(S.a(ic,:).*T.^S.Esp(ic,:));
• $\frac{\bar{h}}{\bar{R}T} = -a_1 T^{-2} + a_2 \frac{\ln T}{T} + a_3 + a_4 \frac{T}{2} + a_5 \frac{T^2}{3} + a_6 \frac{T^3}{4} + a_7 \frac{T^4}{5} + b_1 \frac{1}{T}$
dum=S.Esp(ic,:)~=-1;
dum1=S.a(ic,dum)./(S.Esp(ic,dum)+1).*T.^S.Esp(ic,dum);
dum2=S.a(ic,~dum)*log(T)/T;
H_RT=(sum(dum1)+sum(dum2)+S.b(ic,1)/T);
• $\frac{\bar{S}}{\bar{R}} = -a_1 \frac{T^{-2}}{2} - a_2 T^{-1} + a_3 \ln T + a_4 T + a_5 \frac{T^2}{2} + a_6 \frac{T^3}{3} + a_7 \frac{T^4}{4} + b_2$
dum=S.Esp(ic,i) =0;

dum=S.Esp(1c,:)~=0; dum1=S.a(ic,dum)./(S.Esp(ic,dum)).*T.^S.Esp(ic,dum); dum2=S.a(ic,~dum)*log(T); S_R=(sum(dum1)+sum(dum2)+S.b(ic,2));

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Camera di combustione

```
function [T2n n2]=ReazioneTP(T2,T1,n,n1,p,Rea,Bil, S)
Tf=298.15; R=8314.5;
NSpe=numel(S);
for i=NSpe:-1:1
   [cp_R(i) H_RT(i) S_R(i)] = TermoCea(T1,S(i));
end
H1=H_RT*R*T1;
for i=NSpe:-1:1
   [cp_R(i) H_RT(i) S_R(i)]=TermoCea(T2,S(i));
end
H2=H RT*R*T2:
cpm2=(H2-[S(:).DH0]*1000)/(T2-Tf);
K=exp(sum((H_RT-S_R).*-Rea,2));
options = optimset('Display', 'off', 'Tolx', 1e-18, 'TolFun', 1e-18);
n2=fsolve(@Reazione, n,options ,p ,K ,Rea, Bil);
chi2=n2/sum(n2);
ntot2=sum(n2);
cpmm2=sum(chi2.*cpm2);
T2n=Tf-(sum(n2.*[S(:).DH0]*1000)-sum(n1.*H1))/(ntot2*cpmm2);
```



```
% H2O2Cea.m
clear
         2 3 4
%
       1
                        5
                           6
Spe={'H2O', 'H2', 'O2', 'OH', 'O', 'H'};
               -0.5
Rea=[
       0
           0
                     0
                          1
                            0:
         -0.5
                0
                     0
                            1;
       0
                          0
         -0.5 -0.5 1
                          0
                            0;
       0
        -1 -0.5
                     0
       1
                          0 0];
       2 2
                     1
Bi]=[
                0
                               2*1/1.00794;
                             1
                          0
                2
                     1
       1
                                1*16/15.9994];
           0
                         1 0
          .1
       4
                         .1 .1];
                     .1
               0.1
n= [
             0.5
                         0 0];
n1 =[
         1
                     0
       0
T1=298.15;
%T1=350;
T2 =3000;
p=20*1.013;
```



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Camera di combustione

fprintf('\nT2=%g \n', T2);

```
% H2O2Cea.m
. . .
NSpe=numel (Spe);
for i=NSpe:-1:1
   S(i)=LeggiFileCea(strcat(Spe{i},'.txt'));
end
% T e p assegnati
[~, n2 ]=ReazioneTP(T2,T1,n,n1,p,Rea,Bil, S);
fprintf('csi= ');fprintf('%.4g ',n2/sum(n2));
% adiabatica p assegnato
FunErr=@(T2) ReazioneTP(T2,T1,n,n1,p,Rea,Bil, S)-T2;
options = optimset('Display', 'off', 'Tolx', 1e-18, 'TolFun', 1e-18);
T2=fsolve(FunErr,T2,options );
%T2=fzero(FunErr,T2,options);
[T2 n2 ]=ReazioneTP(T2,T1,n,n1,p,Rea,Bil, S);
fprintf('csi= ');fprintf('%.3g ',n2/sum(n2));
```

https://cearun.grc.nasa.gov/

Enter a 4-character alphanumeric code of your own choosing: 5896

Problem type:

 $\bigcirc hp \ \bigcirc rocket \ \textcircled{o}tp \ \bigcirc det \ \bigcirc sp \ \bigcirc tv \ \bigcirc uv \ \bigcirc sv \ \bigcirc shock$

Output:

 \bigcirc long \bigcirc debug \circledast short

Output:

Output species:

 \odot mole fraction \bigcirc mass fraction

Ions:

Transport properties:

⊖Y⊚N Submit Reset

Dove hp -> adiabatica e p assegnata. tp -> T e P assegnate

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Camera di combustione

You have chosen problem type = tp

Please type in up to 8 temperatures and 8 pressures: (blank boxes are OK)





This is the reactants selection page

Choose your reactants here

Reactant:

 $\odot\, Air \odot RP\text{-}1 \, \odot\, Jet\text{-}A(L) \odot\, CH4$ $\odot\, Use$ Periodic Chart

Submit Reset



Reactant selection page

Click on symbols for atoms contained in desired compounds.



15 13 14 16 17 He VIIA ША IVA VA VIA 3A 4A 5A бA 7A

Choose your reactant(s) (ASCII-betical vertically):

 $\Box H \ \Box H2 \ \Box H2(L)$

More reactants?

 $\odot Y \circ N$

Reactant selection page lick on symbols for atoms contained in desired compounds. 15 14 16 17 13 D He IVA VIIA ШΑ VA VIA 4A 5A 7A 3A 6A -5 Ν В С F Be Ο \checkmark П Propulsione Aerospaziale – ES PA - astarita@unina.it

Camera di combustione You have designated 2 molecules in your reaction mix.

Please indicate relative amounts (mass):

| O2 | 16 |
|----|----|
| | |
| H2 | 2 |

Invia richiesta Reimposta

Check if you wish to use special CEA options:

(All boxes empty for none):

□omit ☑only □insert Your choices for 'ONLY' are:



```
Input data
prob case=58965686 tp
    p(atm) = 20
    t,k= 3500
reac
    name 02     wt%= 88.89
    name H2     wt%= 11.11
output trace=1e-5
only H H2O O H2 O2 OH
end
```



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Camera di combustione

Reazione a T=3500K

| REACTANT | WT.FRAC | (ENERGY/R),K | TEMP,K | DENSITY | EXPLODED FORMULA |
|----------|----------|--------------|--------|---------|------------------|
| N: 02 | 0.888900 | 0.00000E+00 | 0.00 | 0.0000 | o 2.00000 |
| N: H2 | 0.111100 | 0.00000E+00 | 0.00 | 0.0000 | н 2.00000 |

| THERMODYNAMIC P | ROPERTIES | Cp, KJ/(KG)(K) | 12.9454 |
|-----------------|-----------|----------------|----------|
| | | GAMMAS | 1.1254 |
| P, BAR | 20.265 | SON VEL,M/SEC | 1453.0 |
| Т, К | 3500.00 | | |
| RHO, KG/CU M | 1.0802 0 | MOLE FRACTIONS | |
| Н, КЈ/КG | 109.77 | | |
| U, KJ/KG | -1766.33 | *Н | 4.7764-2 |
| G, KJ/KG | -57863.7 | *H2 | 1.3220-1 |
| S, KJ/(KG)(K) | 16.5638 | Н2О | 6.4164-1 |
| | | *0 | 2.2364-2 |
| M, (1/n) | 15.511 | *OH | 1.1429-1 |
| (dLV/dLP)t | -1.05824 | *02 | 4.1743-2 |
| (dLV/dLT)p | 2.0240 | | |



```
Input data
prob case=44623075 hp p(atm)=20
phi=1
reac
fuel H2 wt%= 100.0 t,k= 298.15
oxid 02 wt%= 100.0 t,k= 298.15
output short
output trace= 1e-5
only H H20 0 H2 02 OH
end
```



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Camera di combustione

Reazione adiabatica

| REACTANT | WT FRACTION | ENERGY T | EMP |
|-----------------------|--------------------------------------|-----------------------------------|---------------------|
| FUEL H2 OXIDANT O2 | (SEE NOTE) 1.0000000 1.0000000 | KJ/KG-MOL 0.000 29 0.000 29 | к 8.150 8.150 |
| 0/F= 7.93668 | 8 %FUEL= 11.189834 | R,EQ.RATIO= 1.0 | 00000 PHI,EQ.RATIO= |
| 1.000000 | | | |
| | | | |
| THERMODYNAMIC PR | ROPERTIES | Ср, КЈ/(КG)(К) | 12.8800 |
| | | GAMMAS | 1.1253 |
| P, BAR | 20.265 | SON VEL,M/SEC | 1452.8 |
| Т, К | 3491.86 | | |
| RHO, KG/CU M | 1.0804 0 | MOLE FRACTIONS | |
| H, KJ/KG | 0.00000 | | |
| U, KJ/KG | -1875.66 | *H | 4.7123-2 |
| G, KJ/KG | -57941.0 | *H2 | 1.3352-1 |
| S, $KJ/(KG)(K)$ | 16.5932 | н2о | 6.4615-1 |
| , | | *0 | 2.1406-2 |
| M, (1/n) | 15.479 | *OH | 1.1194-1 |
| (dLV/dLP)t | -1.05735 | *02 | 3.9854-2 |
| (dLV/dLT)p | 2.0110 | | |



Compressori MA9.12

Air enters a compressor stage that has the following properties:

$$\dot{m} = 50 \text{ kg/s}, \quad \omega = 800 \text{ rad/s}, \quad r = 0.5 \text{ m}$$

 $M_1 = M_3 = 0.5, \quad \alpha_1 = \alpha_3 = 40 \text{ deg}, \quad T_{t1} = 290 \text{ K}$
 $P_{t1} = 101.3 \text{ kPa}, \quad u_2/u_1 = 1.0, \quad T_{t3} - T_{t1} = 45 \text{ K}$
 $\phi_{cr} = 0.10, \quad \phi_{cs} = 0.03, \quad \sigma = 1$

Note: For air, use $\gamma = 1.4$ and R = 0.286 kJ/(kg·K). Make and fill out a table of flow properties like Table 9.3, and determine the diffusion factors, degree of reaction, stage efficiency, polytropic efficiency, and flow areas and associated hub and tip radii at stations 1, 2, and 3.



Turbine MA9.35

Products of combustion enter a turbine stage with the following properties:

$$\dot{m} = 40 \text{ kg/s}, \quad T_{t1} = 1780 \text{ K}, \quad P_{t1} = 1.40 \text{ MPa}, \quad M_1 = 0.3$$

 $M_2 = 1.15, \quad \omega r = 400 \text{ m/s}, \quad T_{t3} = 1550 \text{ K}, \quad \alpha_1 = \alpha_3 = 0$
 $r_m = 0.4 \text{ m}, \quad u_3/u_2 = 1.0, \quad \phi_{t \text{ stator}} = 0.04, \quad \phi_{t \text{ rotor}} = 0.08$

Note: For the gas, use $\gamma = 1.3$ and $R = 0.287 \text{ kJ/(kg} \cdot \text{K})$. Make and fill out a table of flow properties like Table 9.12 for the mean line, and determine the degree of reaction, total temperature change, stage efficiency, polytropic efficiency, and flow areas and associated hub and tip radii at stations 1, 2, and 3.



Razzi

MA Example 3.3

Consider both a two-stage vehicle and a three-stage vehicle for the launch of the 900-kg (2000-lbm) payload. Each stage uses a liquid H₂ -O₂ chemical rocket (C ¹/₄ 4115 m/s, 13,500 ft/s), and the DV total of 14,300 m/s (46,900 ft/s) is split evenly between the stages. Suppose $\delta = m_{str}/m_0 = 0.03$.

Mattingly example 3.7

The space shuttle main engine (SSME) operates for up to 520 s in one mission at altitudes over 100 miles. The nozzle expansion ratio 1 is 77:1, and the inside exit diameter is 2.30m. Assume a calorically perfect. We want to calculate the following:

- Characteristic velocity *c**
- Mass flow rate of gases through the nozzle.
- Pressure at which the nozzle is "on-design."
- Pressure at which the nozzle is just separated (assume separation occurs when $p_a > 3.5 p_{r_3}$).
- Thrust coefficient C_F , specific impulse and thrust for $p_0=0$, p_s .

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|---|---|

Razzi

Farokhi problem 12.2

A solid rocket motor has a design chamber pressure of 10 MPa, an end-burning grain with n = 0.4 and $\dot{r} = 3$ cm/s at the design chamber pressure and design grain temperature of 15C. The temperature sensitivity of the burning rate is $\sigma_p = 0.002$ /C, and chamber pressure sensitivity to initial grain temperature is $\pi_K = 0.005$ /C. The nominal effective burn time for the rocket is 120 s, i.e., at design conditions. Calculate:

- the new chamber pressure and burning rate when the initial grain temperature is 75C;
- the corresponding reduction in burn time Δt_b in seconds.



2.298

1.25

2.068E+07

4083

602.6

5.092

m

Pa

Κ

J/kgK

69

De

g

pt

Tt

R

M2

Razzi

Farokhi problem 12.20

Consider a scramjet in a Mach 6 flight. The fuel for this engine is hydrogen with Q_R =120,000kJ/kg. The inlet uses multiple oblique shocks with a total pressure recovery following MIL-E-5008B standards for M0 > 5, i.e.,

$$\pi_d = \frac{800}{M_0^4 + 935}$$

The combustor entrance Mach number is M2=2.6. Use frictionless, constant-pressure heating, i.e., p4=p2, to simulate the combustor with combustor exit Mach number M4= 1.0. All component parameters and gas constants are shown in the schematic drawing below. Calculate:



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Razzi

Farokhi problem 12.20

- (a) Inlet static temperature ratio T2/T0
- (b) combustor exit temperature T4 in K
- (c) fuel-to-air ratio f
- (d) nozzle exit Mach number M10
- (e) nondimensional ram drag Dram/p0A1 (note that A0= A1)
- (f) nondimensional gross thrust Fg/p0A1
- (g) fuel-specific impulse Is in seconds
- (h) combustor area ratio A4/A2
- (i) nozzle area ratio A10/A4
- (j) thermal efficiency
- (k) propulsive efficiency

